

CLAIM AMENDMENTS

Amended claims: 1,2, 4-6. Cancel claim 3.

1. (Currently Amended) A process ~~Process~~ for the preparation of a gas containing hydrogen and carbon monoxide ~~containing gas~~ from a carbonaceous feedstock, the process comprising ~~by performing the following steps:~~
- (a) ~~partial oxidation of~~ partially oxidizing a carbonaceous feedstock in an a vertically oriented tubular partial oxidation reactor vessel having an upper end, and a lower end having an inlet, the vessel comprising a burner at its the upper end thereby obtaining a first gaseous product of hydrogen and carbon monoxide having a temperature between 1100 °C and 1500 °C~~[[,]]~~;
 - (b) ~~catalytic~~ catalytically steam reforming a carbonaceous feedstock in the presence of steam in a ~~Convective Steam-Reformer Zone~~ convective steam reformer zone thereby obtaining a steam reformer product~~[[,]]~~;
 - (c) reducing the temperature of the first gaseous product of step (a) by between 300 °C and 750 °C by mixing ~~this~~ the first gaseous product with the steam reformer product of step (b) by feeding the steam reformer product into the said inlet yielding a first mixture;
 - (d) contacting the first mixture obtained in step (c) with a bed of reforming catalyst positioned in the lower end of the partial oxidation reactor vessel just below the position said inlet and obtaining a second mixture having a temperature between 950 °C and 1100 °C at which the steam-reformer product is fed to said reactor; and
 - (e) providing ~~the required~~ heat for the convective steam reforming reaction zone in step (b) by convective heat exchange between the second mixture obtained in step (d) having a temperature between 950 °C and 1100 °C and the steam reformer reactor zone thereby obtaining a hydrogen and carbon monoxide containing gas having a reduced temperature.
2. (Currently Amended) The process of ~~Process~~ according to claim 1, wherein the steam to carbon molar ratio of the feed to step (b) is between 0.5 and 0.9.

3. Cancel.

4. (Currently Amended) The process ~~Process according to any~~ of claims 1 [[-3]], wherein the content of methane in the steam reformer product is between 1 mol% and 10 mol% relative to the carbon present as hydrocarbon in the carbonaceous feed to step (b).

5. (Currently Amended) The process ~~Process according to~~ of claims 1 [[-4]], wherein the methane conversion in step (d) is between 10 wt% and 50 wt%.

6. (Currently Amended) The process ~~Process according to~~ ~~Process according to any one~~ of claims 1 [[-5]], wherein the temperature of the mixture obtained in step (d) is between 980 °C and 1050 °C.